Comparison of Ethene and Ethane Primary Selectivities with Li/MgO and MgO Catalysts for Oxidative Coupling of Methane: Comments on the Role of Lithium

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The catalysts in the title demonstrate significantly different primary selectivities for ethene and ethane which indicates that Li inhibits the oxidative dehydrogenation activity of MgO.

The oxidative coupling of methane to form ethene and ethane continues to receive considerable research attention. To date most of this research effort has been directed at the identification of suitable catalytic materials, and the mechanism of ethene and ethane formation has received only limited attention. **A** large number **of** oxide catalysts have been proposed for this reaction,^{1,2} and high C_2 selectivities have been observed with catalysts based on $Mg\overline{O}^{3-5}$ and rare earth oxides, $6-8$ particularly Sm_2O_3 .⁹ Recently MnO based catalysts¹⁰ have been shown to give very high yields of C_2 hydrocarbon products. The C_2 selectivity of these catalysts is enhanced significantly by the addition of alkali promoters,¹¹ but the specific catalytic role of such promotion has not yet been delineated, although it has been proposed⁴ that $Li+O^$ centres are the active and selective methane activation centres for Li-promoted MgO catalysts. We have now addressed this problem and in this communication we present our initial findings concerning the role of Li promotion in MgO catalysts as revealed by comparison of primary selectivity data.

MgO was prepared as previously described12 and *5%* Li/MgO was prepared using the method of Lunsford.4 Catalysts were calcined **(24** h, 500°C) prior to use for partial methane oxidation with O_2 as previously described.¹¹

Experiments were conducted for a wide range of reactant flowrates at 710 °C using a fixed CH₄/O₂ molar ratio of 3.5. Variation of ethene and ethane selectivity with increasing reactant feedrates demonstrated significantly different behav-

Table 1. Specific activity data, 710 °C, GHSV 2400 h⁻¹.

 $10⁴$ Specific activity/mol product m⁻² h⁻¹

Catalyst						H_2 , CO, CO, C ₂ H ₄ , C ₂ H ₆ , Total C ₂ , Total C	
Li/MgO	7.7			16.1 1.3 2.5 8.0		10.5	27.9
MgO	3.7	4.5	1.3	0.8	0.8	1.6	7.4

Figure 1. Selectivity vs. reciprocal GHSV: (a) MgO; (b) Li/MgO; \triangle ethane; \bigcirc ethene.

iour for Li/MgO compared to MgO, as shown in plots of selectivity vs. reciprocal gas hourly space velocity (\overline{GHSV} = volumetric gas flow rate/unit catalyst volume/h). With MgO as catalyst (Figure 1a) both ethene and ethane selectivities increase with decreasing reciprocal GHSV, and extrapolation indicates similar primary selectivity (selectivity extrapolated to zero conversion) for both products. Addition of Li (Figure 1b) dramatically changes this behaviour and now ethene selectivity decreases with decreasing reciprocal GHSV. Hence, Li/MgO catalysts demonstrate high ethane primary selectivity but significantly lower ethene primary selectivity when compared to the unpromoted MgO. However, Li addition significantly enhances total C_2 hydrocarbon selectivity (Figure 2) at all reaction conditions investigated as has been previously noted.¹¹ Further experimental evidence can be obtained from comparison of the specific activity data for the two catalysts (Table 1). Addition of Li to MgO significantly enhances the specific activity for all observed products, and also enhances the formation of selective oxidation products. In particular, the specific activity for ethane formation is enhanced by a factor of ca. 3 compared to the enhancement of ethene formation.

Figure 2. Selectivity to total C_2 hydrocarbon vs. reciprocal GHSV: \times Li/MgO; \Box MgO.

It is clear from these data that addition of Li to MgO significantly promotes specific activity in addition to enhancing selectivity to partial oxidation products. The specific role of Li would appear to be the inhibition of oxidation activity of MgO in two ways: (a) by suppressing the activity for the oxidative dehydrogenation of ethane as evidenced by higher primary ethane selectivity for Li/MgO; and (b) by reducing the extent of total oxidation of both ethene and ethane as evidenced by a less pronounced loss of C_2 selectivity with increasing reciprocal space velocity (Figure 2). This is unfortunate, with respect to the industrial application of this catalyst system, since ethene is the more desired reaction product. Studies are now in progress to determine if this is a general feature of alkali addition to active oxide catalysts, and if this is observed then it is apparent that further catalyst modifications will be required to enhance ethene formation.

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